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# Two-phase nanofluid over rotating disk with exponential variable thickness

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## Abstract

**Purpose** - The purpose of this paper is to investigate the effect of nanofluid over rotating disk with the exponential variable thickness  $Z = ce^{-\frac{bR}{R_0}}$ , ( $c > 0, b > 0$ ) and to analyze Brownian motion and thermophoresis of Buongiorno model on the disk embedded in nanofluid-saturated porous media.

**Design/methodology/approach** - Employing the generalized Von Karman transformation, the boundary layer governing equations are transformed into semi-similar forms solved by bvp4c in Matlab.

**Findings** - The effects of the thickness parameter  $a$ , the shape parameter  $b$ , the Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$  on flow, heat and mass transfer are analyzed. With the increase of thickness parameter  $a$ , the radial velocity first decreases and then increases, showing the opposite trend on the two sides of the peak value. Moreover, temperature and concentration rise as the Brownian motion parameter becomes larger.

**Originality/value** - It is the first work that has been done on rotating disk with exponential variable thickness in nanofluid. The impact of the two slip effects, namely, Brownian motion and thermophoresis, on the nanofluid boundary layer flow, heat and mass transfer due to rotating disk with exponential variable thickness  $Z = ce^{-\frac{bR}{R_0}}$ , ( $c > 0, b > 0$ ) has been addressed in this study.

**Keyword** - Variable thickness rotating disk, Nanofluid, Generalized Von Karman transformation, Porous media

**Paper type** - Research paper

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## 1. Introduction

Nanofluid has received wide attention due to its high thermal conductivity and heat transfer capability. The concept of nanofluid was first proposed by Choi and Eastman in 1995

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[1]. Eastman et al. (2001) [2] focused on higher thermal conductivities of ethylene glycol-based nanofluids containing copper nanoparticles instead of oxide nanoparticles. Buongiorno (2006) [3] investigated seven possible slip mechanisms with relative velocity between the nanoparticles and the base fluid and concluded that Brownian motion and thermophoresis are the most important slip mechanisms in nanofluid. The above research stimulated the scholars to Brownian motion and thermophoresis on two-phase nanofluid. Kuznetsov and Nield (2010) [4] studied the natural convective flow of a nanofluid past a vertical plate. Sheikholeslami et al. (2013) [5] depicted two-phase simulation of nanofluid flow and heat transfer. Reddy and Chamkha (2017) [6] studied natural convection flow of nanofluid along a vertical cone with chemical reaction. More literatures on nanofluid flow and heat transfer have been presented in Refs.(Nield and Kuznetsov, 2009; Mohsen et al., 2014; Chamkha et al., 2015; Zhang et al., 2016, 2017; Wakif et al. 2018) [7–11].

The problem of the flow and heat transfer in porous media is important in many industrial fields, such as food processing, geothermal extraction, and diffusion of underground pollutants. Darcy put forward the transport phenomena in porous media for the first time in 1856 (Khayargoli et al, 2004) [12]. Later, Yih (1998) [13] studied the effect of uniform suction/blowing on forced MHD Hiemenz flow in a porous medium against a variable wall temperature plate. Chamkha and Al-Humoud (2007) [14] presented mixed convection of a power-law fluid over a vertical plate embedded in a fluid-saturated porous medium. Hassanien and Al-Arabi (2009) [15] considered the unsteady stagnation point flow near a heated vertical plate in a porous medium. Chamkha et al. (2014) [16] investigated heat and mass transfer with Soret and Dufour effects through a porous medium under the inclined magnetic field. Barnoon and Toghraie (2018) [17] showed heat transfer of kerosene/MWCNT nanofluid in a double-layer microchannel through a porous medium.

Flow induced by the rotation of disk has been used in the field of engineering and technology such as turbine, aircraft propeller, and centrifugal pump. The governing equations of steady flow on rotating disk were originally reduced to similarity forms by Karman (1921) [18]. Based on this work, Millsaps and Pohlhausen (1951) [19] considered laminar flow and heat transfer from a rotating-plate by Keller box method. Ackroyd (1978) [20] investigated series solution of rotating disk flow with either surface suction or injection. The influence of porous media on the steady flow due to a rotating disk was examined in (Turkyilmazoglu, 2010; Devi and Devi, 2012; Rashidi et al., 2013; Khan et al., 2016) [21–24]. The fluid flow model on the rotating disk is more mature.

Recently, Xun et al. (2016) [25] studied power-law fluids over a variable thickness rotating disk with index decreasing by Runge-Kutta method coupled with multi-shooting technique. Hayat et al. (2017) [26] reported nanofluid flow with homogeneous-heterogeneous reactions due to rotating disk with variable thickness through the homotopy analysis method (HAM). Several recent studies on the modeling of variable thickness rotating disk with index decreasing have been discussed by Hayat et al. (2017; 2018; 2018) [27–29]. On the other hand, Liu et al. (2016) [30] investigated approximate analytical solutions of Bingham fluid over a variable thickness rotating disk with exponential decreasing by HAM. The above-mentioned works are based on the similarity transformation method, and then numerical or analytical solutions are obtained to solve a set of ordinary differential equations. Also there exist some

novel methods which can be used to solve the boundary layer problems directly (Mirzaei and Dehghan, 2012; Dehghan and Abbaszadeh, 2016; 2017; Kamranian et al., 2017; Dehghan and Abbaszadeh, 2018)[31–35]. To the best of our knowledge, very few studies have been conducted for investigating rotating disk with exponential variable thickness flow problems.

Motivated by the discussions mentioned above, it is meaningful to investigate flow, heat and mass transfer of two-phase nanofluid model over rotating disk with exponential variable thickness in porous media. Boundary layer governing partial equations are solved by the generalized Von Karman transformation and `bvp4c` in Matlab. Impacts of pertinent parameters on velocity, temperature and concentration fields are discussed by displaying figures and tables. Moreover, physical quantities at the disk (local Nusselt number and local Sherwood number) are discussed graphically. The structure of the paper is as follows:

In Section 2, the governing equations of model and generalized Von-Karman transformations are highlighted.

In Section 3, the numerical results and discussions are given.

Finally, the conclusions are eventually summarized in Section 4.

## Nomenclature

$a$	=thickness parameter, ( $a > 0$ ), $[-]$
$b$	=shape parameter, ( $b > 0$ ), $[-]$
$c$	=variable thickness parameter, $[m]$
$C$	=concentration, $[kg\ m^{-3}]$
$C_{fr}$	=local skin-friction coefficient, $[-]$
$C_\infty$	=ambient concentration, $[kg\ m^{-3}]$
$D_B$	=Brownian diffusion coefficient, $[m^2\ s^{-1}]$
$D_T$	=thermophoretic diffusion coefficient, $[m^2\ s^{-1}]$
$k$	=thermal conductivity, $[W\ m^{-1}\ K]$
$K$	=permeability of porous medium, $[m^2]$
$M$	=permeability parameter, $[-]$
$Nb$	=Brownian motion parameter, $[-]$
$Nt$	=thermophoresis parameter, $[-]$
$Nu_r$	=local Nusselt number, $[-]$
$P$	=pressure, $[Pa]$
$Pr$	=Prandtl number, $[-]$
$q_m$	=mass flux, $[kg\ m^{-2}\ s^{-1}]$
$q_w$	=heat flux, $[W\ m^{-2}]$
$R_0$	=feature radius, $[m]$
$Re$	=Reynolds number, $[-]$
$Sc$	=Schmidt number, $[-]$
$Sh_r$	=local Sherwood number, $[-]$
$T$	=temperature, $[K]$
$T_W$	=temperature of disk, $[K]$
$T_\infty$	=ambient temperature, $[K]$
$(U, V, W)$	=velocity in $R, \Phi, Z$ -axis direction, $[m\ s^{-1}]$
$(R, \Phi, Z)$	= $R, \Phi, Z$ -axis, $[m]$
<i>Greek symbols</i>	
$(\rho c_p)_f, (\rho c_p)_s$	=heat capacity of fluid, nanoparticle, $[kg\ m^{-3}\ K]$
$\tau_{rz}, \tau_{\phi z}$	=radial stress, tangential stress, $[N]$
$\tau$	=nanoparticle heat capacity ratio, $[-]$
$\eta$	=similarity variable, $[-]$
$\xi$	=similarity variable after coordinate transformation, $[-]$
$\mu$	=dynamic viscosity, $[Ns\ m^{-2}]$
$\rho$	=density, $[kg\ m^{-3}]$
$\omega$	=constant angular velocity, $[s^{-1}]$
<i>Subscripts</i>	
$W$	=condition at the disk, $[-]$
$\infty$	=ambient condition, $[-]$
$f$	=fluid, $[-]$
$s$	=nanoparticle, $[-]$
<i>Superscripts</i>	
$'$	=differentiation with respect to $\eta$ or $\xi$ , $[-]$

## 2. Mathematical model

Consider the steady incompressible three-dimensional flow of two-phase nanofluid on a radially variable thickness rotating disk with exponential decreasing form  $Z = ce^{-\frac{bR}{R_0}}$ , ( $c > 0, b > 0$ ) shown in Fig. 1, where  $c$  is the variable thickness parameter of disk,  $b$  is the shape parameter of disk. The disk embedded in nanofluid-saturated porous media is rotating about the  $Z$ -axis with constant angular velocity  $\omega$  in the cylindrical coordinate system  $(R, \Phi, Z)$ . The continuity equation, momentum equation, energy equation and mass transfer equation in the boundary layer can be written as follows

$$\frac{\partial U}{\partial R} + \frac{U}{R} + \frac{\partial W}{\partial Z} = 0 \quad (1)$$

$$\rho \left( U \frac{\partial U}{\partial R} + W \frac{\partial U}{\partial Z} - \frac{V^2}{R} \right) = -\frac{\partial P}{\partial R} + \mu \left( \frac{\partial^2 U}{\partial R^2} + \frac{1}{R} \frac{\partial U}{\partial R} - \frac{U}{R^2} + \frac{\partial^2 U}{\partial Z^2} \right) - \frac{\mu}{K} U \quad (2)$$

$$\rho \left( U \frac{\partial V}{\partial R} + W \frac{\partial V}{\partial Z} + \frac{UV}{R} \right) = \mu \left( \frac{\partial^2 V}{\partial R^2} + \frac{1}{R} \frac{\partial V}{\partial R} - \frac{V}{R^2} + \frac{\partial^2 V}{\partial Z^2} \right) - \frac{\mu}{K} V \quad (3)$$

$$\begin{aligned} (\rho c_p)_f \left( U \frac{\partial T}{\partial R} + W \frac{\partial T}{\partial Z} \right) &= k \left( \frac{\partial^2 T}{\partial R^2} + \frac{1}{R} \frac{\partial T}{\partial R} + \frac{\partial^2 T}{\partial Z^2} \right) \\ + (\rho c_p)_s \left( D_B \left( \frac{\partial T}{\partial R} \frac{\partial C}{\partial R} + \frac{\partial T}{\partial Z} \frac{\partial C}{\partial Z} \right) + \frac{D_T}{T_\infty} \left( \left( \frac{\partial T}{\partial R} \right)^2 + \left( \frac{\partial T}{\partial Z} \right)^2 \right) \right) \end{aligned} \quad (4)$$

$$U \frac{\partial C}{\partial R} + W \frac{\partial C}{\partial Z} = D_B \left( \frac{\partial^2 C}{\partial R^2} + \frac{1}{R} \frac{\partial C}{\partial R} + \frac{\partial^2 C}{\partial Z^2} \right) + \frac{D_T}{T_\infty} \left( \frac{\partial^2 T}{\partial R^2} + \frac{1}{R} \frac{\partial T}{\partial R} + \frac{\partial^2 T}{\partial Z^2} \right) \quad (5)$$

The relevant boundary conditions are

$$\begin{aligned} Z = ce^{-\frac{bR}{R_0}} : U = 0, V = \omega R, W = 0, T = T_W, C = C_W \\ Z \rightarrow \infty : U = 0, V = 0, T = T_\infty, C = C_\infty \end{aligned} \quad (6)$$

where  $U$ ,  $V$  and  $W$  are velocity components in the directions of  $R$ ,  $\Phi$ ,  $Z$ , respectively.  $T$  is the temperature,  $C$  is the concentration,  $\rho$  is the density and  $\mu$  is the dynamic viscosity.  $k$  is the thermal conductivity,  $c_p$  is the specific heat of nanofluid,  $K$  is the permeability of the porous media.  $D_B$  is the Brownian diffusion coefficient,  $D_T$  is the thermophoretic diffusion coefficient,  $P$  is the pressure and  $R_0$  is the feature radius.  $T_W$  is the temperature of disk and  $T_\infty$  is the temperature of ambient fluid.  $C_W$  is the concentration of disk and  $C_\infty$  is the concentration of ambient fluid.

The following dimensionless variables are introduced

$$\begin{aligned} r &= \frac{R}{R_0}, z = \frac{Z}{R_0}, u = \frac{U}{\omega R_0}, v = \frac{V}{\omega R_0}, w = \frac{W}{\omega R_0}, t = \frac{T - T_\infty}{T_W - T_\infty}, \\ c' &= \frac{C - C_\infty}{C_W - C_\infty}, Re = \frac{\rho \omega R_0^2}{\mu}, M = \frac{R_0^2}{K}, Pr = \frac{\mu c_p}{k}, \tau = \frac{(\rho c_p)_s}{(\rho c_p)_f}, \\ Nb &= \frac{\tau \rho D_B (C_W - C_\infty)}{\mu}, Nt = \frac{\tau \rho D_T (T_W - T_\infty)}{\mu T_\infty}, Sc = \frac{\mu}{\rho D_B}, p = \frac{P}{\mu \omega} \end{aligned} \quad (7)$$

where  $Pr$  is the Prandtl number,  $Re$  is the Reynolds number,  $Sc$  is the Schmidt number and  $M$  is the permeability parameter.  $Nb$  is the Brownian motion parameter and  $Nt$  is the thermophoresis parameter and  $\tau$  is the ratio between the effective heat capacity of the nanoparticle and heat capacity of the fluid.

Eqs. (1)-(6) are reduced to the following system of equations by using Eq. (7):

$$\frac{\partial u}{\partial r} + \frac{u}{r} + \frac{\partial w}{\partial z} = 0 \quad (8)$$

$$Re \left( u \frac{\partial u}{\partial r} + w \frac{\partial u}{\partial z} - \frac{v^2}{r} \right) = -\frac{\partial p}{\partial r} + \frac{\partial^2 u}{\partial r^2} + \frac{1}{r} \frac{\partial u}{\partial r} - \frac{u}{r^2} + \frac{\partial^2 u}{\partial z^2} - Mu \quad (9)$$

$$Re \left( u \frac{\partial v}{\partial r} + w \frac{\partial v}{\partial z} + \frac{uv}{r} \right) = \frac{\partial^2 v}{\partial r^2} + \frac{1}{r} \frac{\partial v}{\partial r} - \frac{v}{r^2} + \frac{\partial^2 v}{\partial z^2} - Mv \quad (10)$$

$$\begin{aligned} Re \left( u \frac{\partial t}{\partial r} + w \frac{\partial t}{\partial z} \right) &= \frac{1}{Pr} \left( \frac{\partial^2 t}{\partial r^2} + \frac{1}{r} \frac{\partial t}{\partial r} + \frac{\partial^2 t}{\partial z^2} \right) \\ + Nb \left( \frac{\partial t}{\partial r} \frac{\partial c'}{\partial r} + \frac{\partial t}{\partial z} \frac{\partial c'}{\partial z} \right) &+ Nt \left( \left( \frac{\partial t}{\partial r} \right)^2 + \left( \frac{\partial t}{\partial z} \right)^2 \right) \end{aligned} \quad (11)$$

$$ReSc \left( u \frac{\partial c'}{\partial r} + w \frac{\partial c'}{\partial z} \right) = \left( \frac{\partial^2 c'}{\partial r^2} + \frac{1}{r} \frac{\partial c'}{\partial r} + \frac{\partial^2 c'}{\partial z^2} \right) + \frac{Nt}{Nb} \left( \frac{\partial^2 t}{\partial r^2} + \frac{1}{r} \frac{\partial t}{\partial r} + \frac{\partial^2 t}{\partial z^2} \right) \quad (12)$$

subject to the boundary conditions

$$\begin{aligned} z = ae^{-br} : u &= 0, v = r, w = 0, t = 1, c' = 1 \\ z \rightarrow \infty : u &= 0, v = 0, t = 0, c' = 0 \end{aligned} \quad (13)$$

where  $a = c/R_0$  is the variable thickness parameter.

Consider the generalized Von-Karman transformations

$$\eta = e^{br} z, u = rF(\eta), v = rG(\eta), w = e^{-br}H(\eta), t = \varphi(\eta), c' = \theta(\eta) \quad (14)$$

where  $\eta$  is similarity variable. Substituting Eq. (14) in Eqs. (8)-(13), we obtain the following system of semi-similarity equations:

$$2F + rF'b\eta + H' = 0 \quad (15)$$

$$\text{Re} (F^2 + rFF'b\eta + HF' - G^2) = (b + \frac{3}{r})F'b\eta + F'' (b^2\eta^2 + e^{2br}) - MF \quad (16)$$

$$\text{Re} (rFG'b\eta + G'H + 2FG) = (b + \frac{3}{r})G'b\eta + G'' (b^2\eta^2 + e^{2br}) - MG \quad (17)$$

$$\text{Re} (rFb\eta + H) \varphi' = \frac{1}{\text{Pr}} \left( (b^2\eta^2 + e^{2br}) \varphi'' + (b + \frac{1}{r})\varphi'b\eta \right) + \left( Nb\varphi'\theta' + Nt(\varphi')^2 \right) (b^2\eta^2 + e^{2br}) \quad (18)$$

$$\text{ReSc} (rFb\eta + H) \theta' = \left( \theta'' (b^2\eta^2 + e^{2br}) + (b + \frac{1}{r})\theta'b\eta \right) + \frac{Nt}{Nb} \left( \varphi'' (b^2\eta^2 + e^{2br}) + (b + \frac{1}{r})\varphi'b\eta \right) \quad (19)$$

The transformed boundary conditions become

$$\begin{aligned} \eta = a : F = 0, G = 1, H = 0, \varphi = 1, \theta = 1, \\ \eta \rightarrow \infty : F = 0, G = 0, \varphi = 0, \theta = 0 \end{aligned} \quad (20)$$

where  $a$  is the thickness parameter, and  $\eta = a$  indicates the rotating disk surface. The prime denotes derivative with respect to  $\eta$ .

In order to facilitate the computation, we define

$$\begin{aligned} F(\eta) = f(\eta - a) = f(\xi), G(\eta) = g(\eta - a) = g(\xi), H(\eta) = h(\eta - a) = h(\xi), \\ \varphi(\eta) = s(\eta - a) = s(\xi), \theta(\eta) = q(\eta - a) = q(\xi) \end{aligned} \quad (21)$$

Eqs.(15)-(20) become

$$2f + rf'b(\xi + a) + h' = 0 \quad (22)$$

$$\text{Re} (f^2 + rff'b(\xi + a) + f'h - g^2) = (b + \frac{3}{r})f'b(\xi + a) + f'' (b^2(\xi + a)^2 + e^{2br}) - Mf \quad (23)$$

$$\text{Re} (rfg'b(\xi + a) + g'h + 2fg) = (b + \frac{3}{r})g'b(\xi + a) + g'' (b^2(\xi + a)^2 + e^{2br}) - Mg \quad (24)$$

$$\begin{aligned} \text{Re} (rfb(\xi + a) + h) s' = \frac{1}{\text{Pr}} \left( (b^2(\xi + a)^2 + e^{2br}) s'' + (b + \frac{1}{r})b(\xi + a) s' \right) \\ + \left( Nbs'q' + Nt(s')^2 \right) (b^2(\xi + a)^2 + e^{2br}) \end{aligned} \quad (25)$$



$$\begin{aligned}
ReSc(rfb(\xi+a)+h)q' &= \left( (b^2(\xi+a)^2+e^{2br})q'' + (b+\frac{1}{r})b(\xi+a)q' \right) \\
&+ \frac{Nt}{Nb} \left( (b^2(\xi+a)^2+e^{2br})s'' + (b+\frac{1}{r})b(\xi+a)s' \right)
\end{aligned} \tag{26}$$

with these boundary conditions

$$\begin{aligned}
f(0) &= 0, g(0) = 1, h(0) = 0, s(0) = 1, q(0) = 1 \\
f(\infty) &= 0, g(\infty) = 0, s(\infty) = 0, q(\infty) = 0
\end{aligned} \tag{27}$$

where the prime denotes the differentiation with respect to the similarity variable  $\xi$ .

Quantities of practical interest in this model are the local skin-friction coefficient  $C_{fr}$ , the local Nusselt number  $Nu_r$  and the local Sherwood number  $Sh_r$ . These are defined by

$$C_{fr} = \frac{\sqrt{\tau_{rz}^2 + \tau_{\phi z}^2}}{\rho(R\omega)^2}, Nu_r = \frac{Rq_W}{k(T_W - T_\infty)}, Sh_r = \frac{Rq_m}{D_B(C_W - C_\infty)} \tag{28}$$

Further the radial stress  $\tau_{rz}$ , tangential stress  $\tau_{\phi z}$ , heat flux  $q_W$  and mass flux  $q_m$  are obtained as follows:

$$\begin{aligned}
\tau_{rz} &= \mu \left( \frac{\partial U}{\partial Z} + \frac{\partial W}{\partial R} \right) \Big|_{Z=ce-\frac{bR}{R_0}}, \tau_{\phi z} = \mu \left( \frac{\partial V}{\partial Z} + \frac{1}{R} \frac{\partial W}{\partial \Phi} \right) \Big|_{Z=ce-\frac{bR}{R_0}}, \\
q_W &= -k \frac{\partial T}{\partial Z} \Big|_{Z=ce-\frac{bR}{R_0}}, q_m = -D_B \frac{\partial C}{\partial Z} \Big|_{Z=ce-\frac{bR}{R_0}}
\end{aligned} \tag{29}$$

Substituting Eq. (29) in Eq. (28), we obtain

$$\begin{aligned}
C_{fr} &= \frac{e^{br} \sqrt{(rf'(0) + e^{-2br}b(ah'(0) - h(0)))^2 + (rg'(0))^2}}{Re r^2}, \\
Nu_r &= -rs'(0)e^{br}, Sh_r = -rq'(0)e^{br}.
\end{aligned} \tag{30}$$

### 3. Results and Discussions

The flow, heat and mass transfer of two-phase model of nanofluid over a rotating disk with variable thickness radially through porous media are studied. The set of nonlinear ordinary differential Eqs. (22)-(27) are solved by bvp4c in Matlab. A comparison among previous results given by Turkiymazoglu (2010) [21], Rashidi et al. (2013) [23] and our results of Newtonian fluid is illustrated in Table 1. An excellent agreement in all results is found. Table 2 presents the used CPU times for the presented method with different  $Re$ . For the sake of simplicity, Prandtl number is 1 and Schmidt number is 1. The effects of other physical parameters, namely permeability parameter  $M$ , thickness parameter  $a$ , shape

parameter  $b$ , Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$  on flow, heat, and mass transfer are discussed.

The variation of the radial velocity profiles for different values of the thickness parameter  $a$  and permeability parameter  $M$  is shown in Fig. 2. With the increase of the thickness parameter  $a$ , the maximum value of the radial velocity profile remarkably reduces, but the thickness of momentum boundary layer increases slightly in Fig. 2 (a). The influence of the permeability parameter  $M$  on the component of radial velocity is depicted in Fig. 2 (b). With the increase of the permeability parameter  $M$ , both radial velocity and thickness of momentum boundary layer decrease.

The dependence of the radial and tangential velocity profiles on different values of the shape parameter  $b$  is shown in Fig. 3. Fig. 3 (a) indicates the radial velocity first decreases and then increases, showing the opposite distribution around the peak value for the increase of shape parameter  $b$ . Moreover, as the shape parameter  $b$  becomes larger, the thickness of the radial velocity boundary layer is thicker and the peak value of the radial velocity is far from the disk. An increase in thickness parameter  $b$  corresponds to larger tangential velocity and thicker thickness of the tangential velocity boundary layer as shown in Fig. 3 (b). That is to say, physically, the increase of the steepness of the disk promotes the radial and tangential velocity.

The variation of the axial velocity profiles for different values of the thickness parameter  $a$  and permeability parameter  $M$  is plotted in Fig. 4. Fig. 4 (a) shows the axial velocity increases with the increase of the thickness parameter  $a$  until it is close to the maximum and is maintained, where the axial velocity decreases with augment of the thickness parameter  $a$ . It is noteworthy that the thickness of axial velocity boundary layer decreases with the thicker disk. Fig. 4 (b) discloses the axial velocity and its boundary layer thickness both decrease with the increase of the permeability parameter  $M$  in the entire boundary layer. From the physical point of view, the flow resistance of porous media restrains the axial velocity.

The dependence of the temperature profiles for different values on the Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$  is shown in Fig. 5, which exhibits that the temperature rises as the increase of Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$ , and the thickness of the thermal boundary layer also becomes thicker, which means that the thermal resistance enlarges.

The variation of the temperature profiles for different values of the thickness parameter  $a$  and shape parameter  $b$  is shown in Fig. 6. It can be obtained from Fig. 6 (a) and (b) that the temperature rises as the thickness parameter  $a$  and thickness parameter  $b$  become larger, which demonstrate a loss of the thickness of the thermal boundary layer. It is worth mentioning that the steepness has a more significant effect on the temperature curve.

The dependence of the concentration profiles for different values on the shape parameter  $b$  and Brownian motion parameter  $Nb$  is shown in Fig. 7. The concentration and the thickness of concentration boundary layer are observed to increase as the magnitude of the shape parameter  $b$  increases in Fig. 7 (a). The effect of Brownian motion parameter  $Nb$  on the concentration profile is displayed in Fig. 7 (b). The result shows that the Brownian motion parameter  $Nb$  enhances the concentration of nanofluid, together with the thickness

of concentration boundary layer.

Fig. 8 shows the variation of the radial and tangential velocity profiles for different values of the Reynolds number. In Fig. 8 (a), the values of the peak of radial velocity increase with the increasing Reynolds number  $Re$ , and its location moves slightly towards the disk. As the Reynolds number increases, the radial velocity boundary layer thickness becomes thinner. It is noted that the tangential velocity distribution shows decreasing behavior corresponding to higher values of Reynolds number. Higher values of the Reynolds number result in the reduction of tangential velocity boundary layer thickness as presented in Fig. 8 (b). Fig. 9 indicates the effects of the Reynolds number for the axial velocity. There is an enhancement in axial velocity near the disk while there is a reduction in axial velocity far away from the disk. It is observed that the boundary layer thickness decreases correspondingly.

Effects of the Reynolds number on temperature and concentration are captured in Fig. 10. There is a reduction in temperature and thermal layer thickness within the frame of Reynolds number  $Re$ . For higher Reynolds number, a reduced concentration of the nanofluid is considered in Fig. 10 (b). Therefore, the thickness of the concentration boundary layer becomes thinner and the ability of mass transfer is enhanced.

In Fig. 11, the variation of the local skin-friction coefficient and the local Sherwood number for different values of the thickness parameter  $a$  and the shape parameter  $b$ . Fig. 11 (a) shows that there is an increase in the local skin-friction coefficient with the increasing values of the thickness parameter  $a$  and shape parameter  $b$ . Fig. 11 (b) displays an increasing trend in the profile of local Sherwood number is observed at all values of the thickness parameter  $a$  and shape parameter  $b$ . A high local Sherwood number indicates that the intensity of fluid convective mass transfer near the disk is enhanced. The change of skin friction coefficient is nonlinear with shape parameter, while the growth of local Sherwood number is the approximately linear correlation.

Fig. 12 illustrates the variation of local Nusselt number and the local Sherwood number for different values of the Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$ . It is evident that the local Nusselt number is seen to be sufficiently reduced for Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$  increase in Fig. 12 (a). However, the local Sherwood number rises as the values of Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$  increase in Fig. 12 (b). It is worth mentioning that the local Sherwood number presents nonlinear growth with the Brownian motion.

Finally, Table 3 describes the effect of thickness parameter  $a$  and shape parameter  $b$  variations on the local Nusselt number. As the thickness parameter  $a$  increase, there is a rise in the local Nusselt number at the disk. But, an increase in the thickness number  $b$  leads to a decrease in local Nusselt number. Physically, a thinner disk with steeper surface results in small heat transfer rate.

#### 4. Conclusions

Boundary layer flow of two-phase nanofluid over a rotating disk with exponential variable thickness in porous media has been studied. The generalized Von Karman transformation

is used to convert the partial differential equations into a system of nonlinear ordinary differential equations that can be solved numerically by bvp4c in Matlab. Comparison with previous solutions is also made to ensure the accuracy and efficiency of the applied numerical technique. Related physical parameters (thickness parameter  $a$ , shape parameter  $b$ , permeability parameter  $M$ , Brownian motion parameter  $Nb$  and thermophoresis parameter  $Nt$ ) are analyzed graphically. Key points of the present study are listed below:

- (I) With the increase of shape parameter  $b$ , the radial velocity first decreases and then increases, showing the opposite trend on the sides of the peak value.
- (II) Temperature rises as both the thickness parameter  $a$  and shape parameter  $b$  become larger.
- (III) Temperature and concentration profiles decline with an increase of Brownian motion parameter  $Nb$ . At the same time, their boundary layers also become thicker.
- (IV) The thickness parameter  $a$  enhances the heat transfer rate of the disk while shape parameter  $b$  decreases the heat transfer rate.

## Acknowledgments

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## Figures

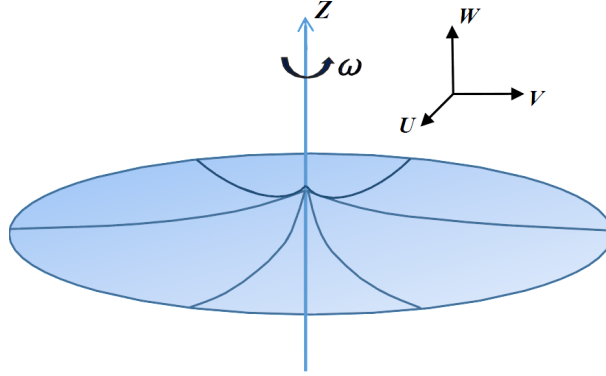


Fig. 1: Schematic diagram of the model.

Table 1: Comparison of  $f'(0)$  for  $b = 0$ ,  $Re = 1$  with the previous works.

$M$	Turkyilmazoglu (2010) [21]	Rashidi et al. (2013) [23]	Present work
0	—	0.510186	0.509450
1	0.309258	0.309237	0.309253
4	0.165703	0.165701	0.165704

Table 2: The used CPU time(s) for the bvp4c and shooting method for momentum equations.

		$Re = 30$	$Re = 35$	$Re = 40$
CPU times (s)	bvp4c	0.089501	0.096779	0.108943
	shooting method	0.095570	0.107075	0.146863

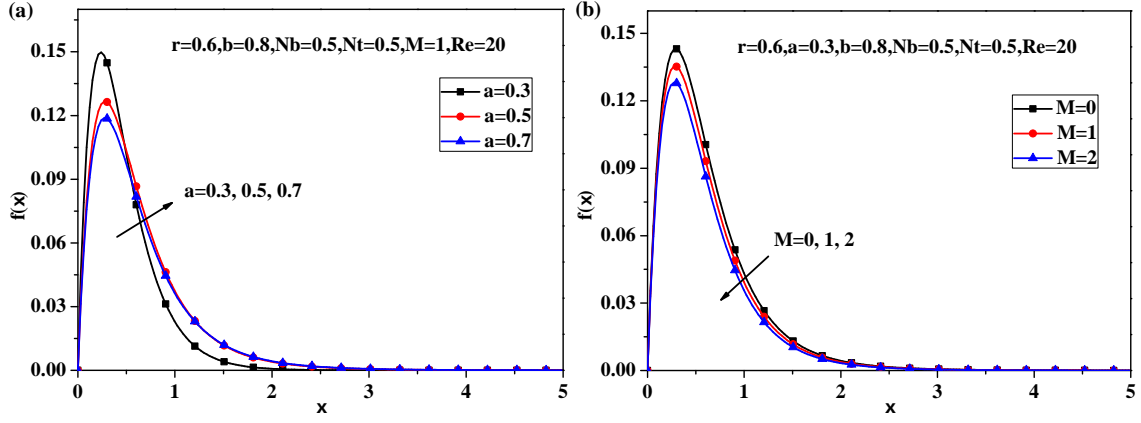


Fig. 2: Radial velocity profiles with the variation of thickness parameter and permeability parameter.

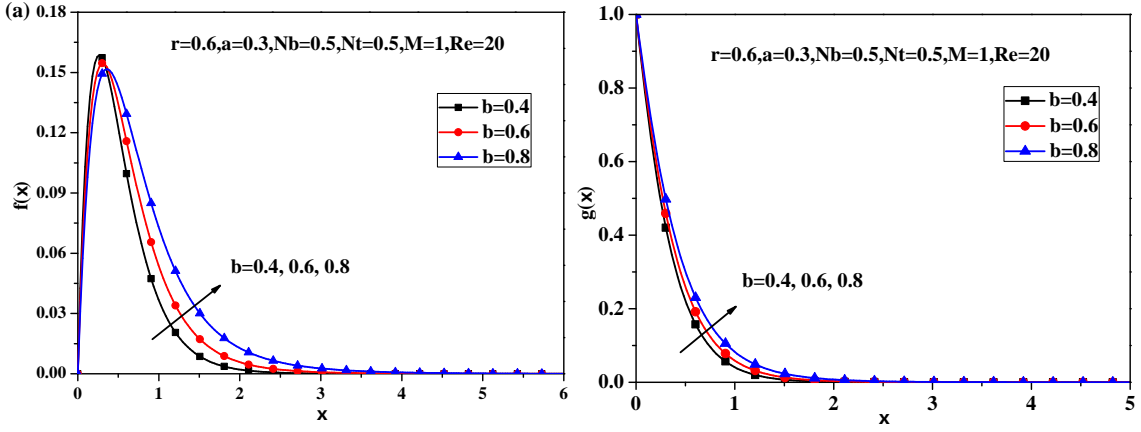


Fig. 3: Radial and tangential velocity profiles with the variation of shape parameter.

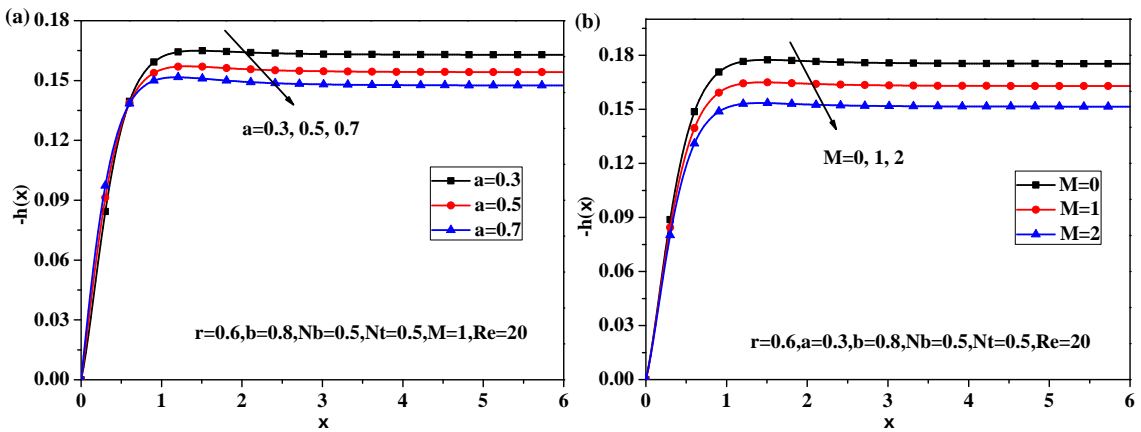


Fig. 4: Axial velocity profiles with the variation of thickness parameter and permeability parameter.



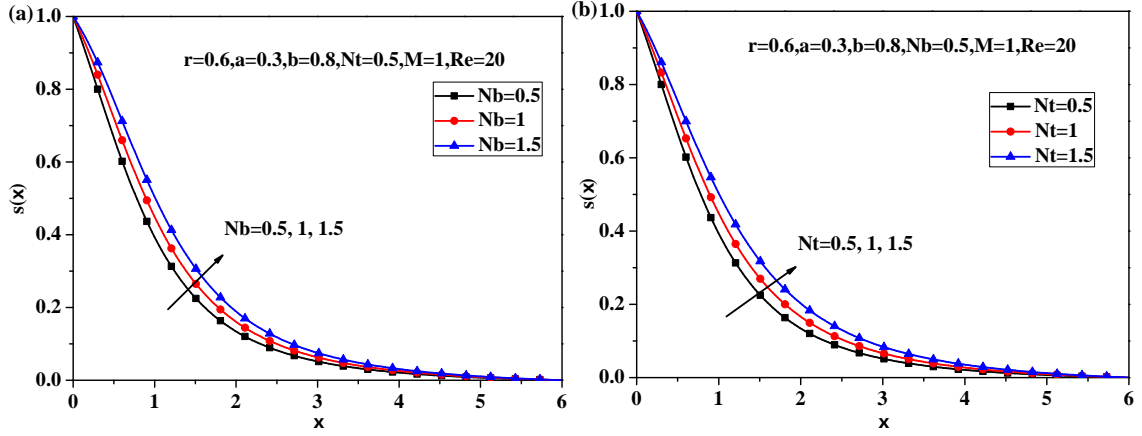


Fig. 5: Temperature profiles with the variation of Brownian motion parameter and thermophoresis parameter.

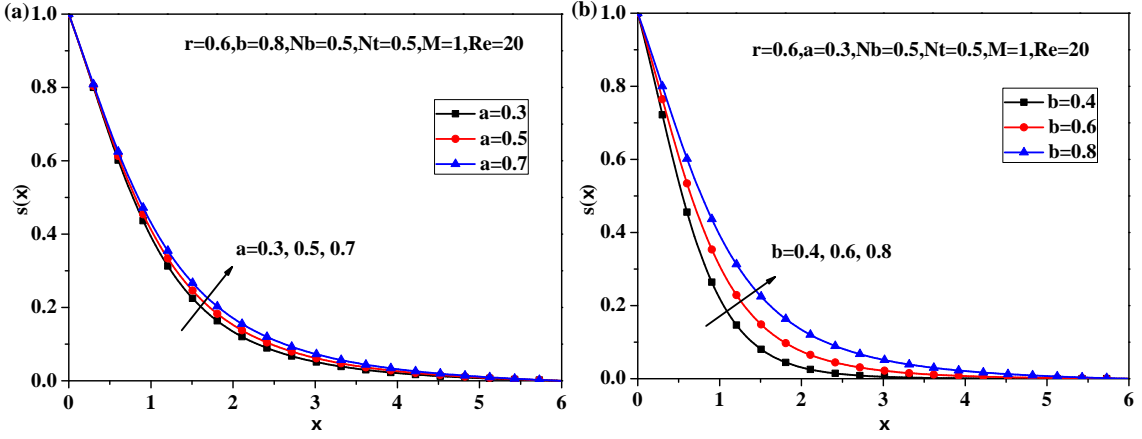


Fig. 6: Temperature profiles with the variation of thickness parameter and shape parameter.

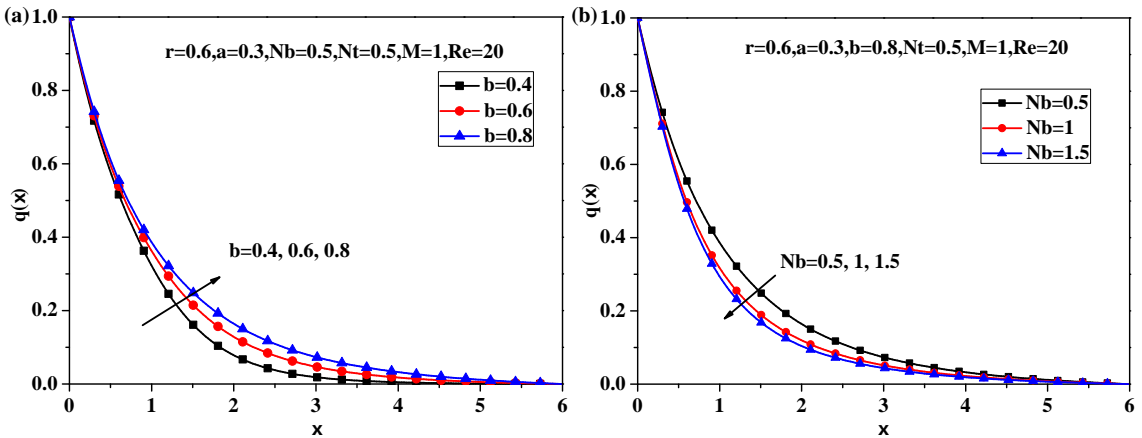


Fig. 7: Concentration profiles with the variation of shape parameter and Brownian motion parameter.

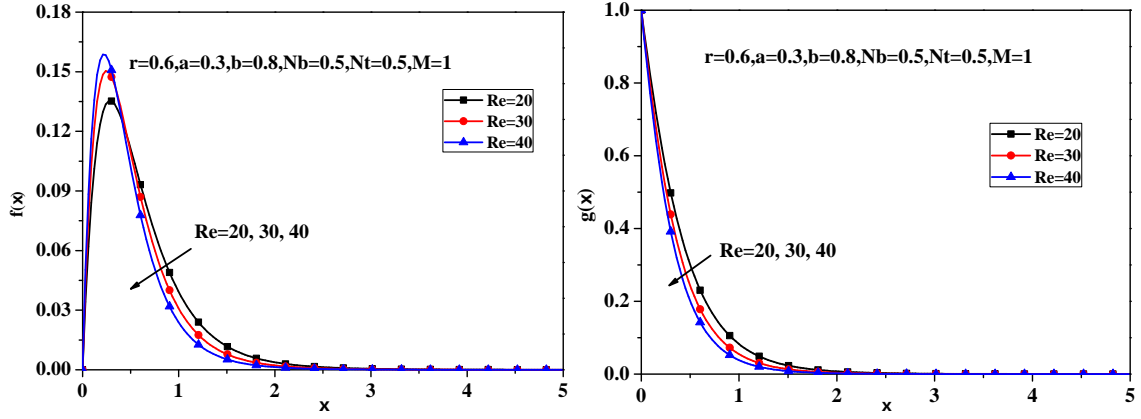


Fig. 8: Radial and tangential velocity profiles with the variation of Reynolds number.

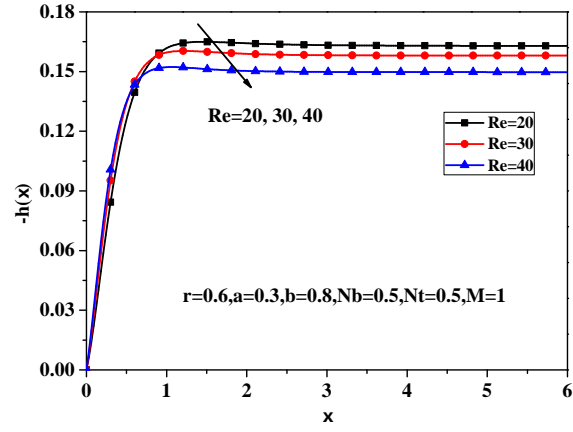


Fig. 9: Axial velocity profiles with the variation of Reynolds number.

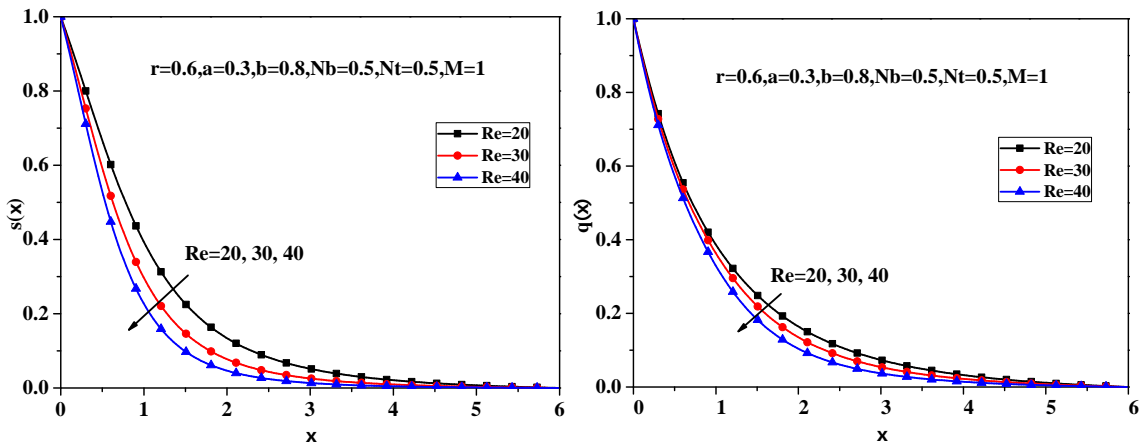


Fig. 10: Temperature and concentration profiles with the variation of Reynolds number.

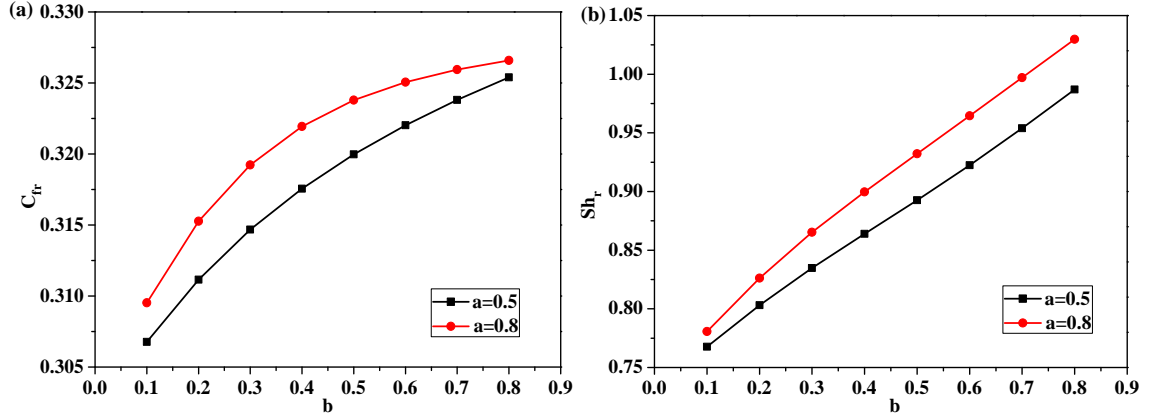


Fig. 11: Physical quantities at the disk with the variation of thickness parameter and shape parameter.

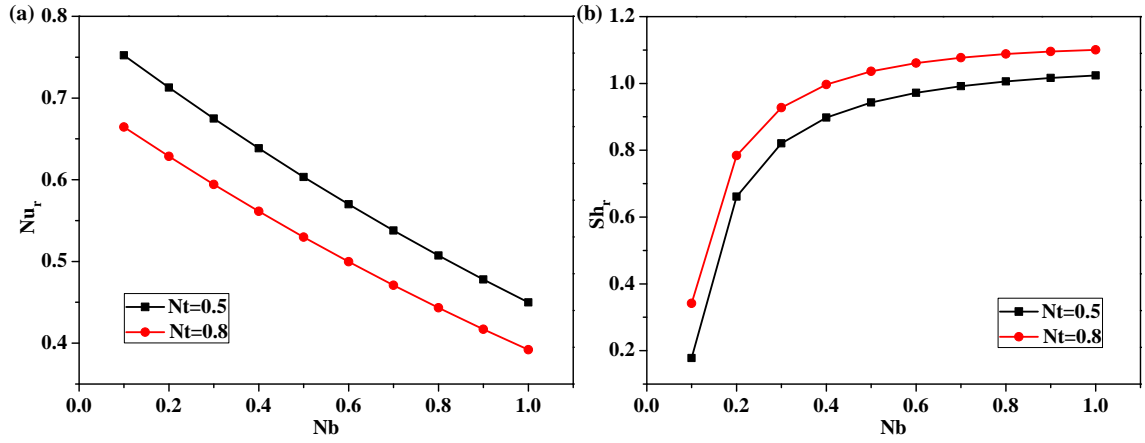


Fig. 12: Physical quantities at the disk with the variation of Brownian motion parameter and thermophoresis parameter.

Table 3: Local Nusselt number  $Nu_r$  for various values of  $a$  and  $b$ .

		$b$				
$Nu_r$		0.1	0.2	0.3	0.4	0.5
$a$	0.3	0.6713	0.66328	0.65428	0.64447	0.63405
	0.5	0.673	0.66543	0.65609	0.64551	0.63419
	0.7	0.67504	0.66689	0.65546	0.64215	0.62816